

Reactor Design II





Week 9 CSTR With Heat Effects

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Introduction



- Chemical Reaction Engineering (CRE) explores reactor design, including heat effects and stability.
- This lecture focuses on Continuous Stirred Tank Reactors (CSTRs) with heat effects, multiple steady states, and the concepts of ignition and extinction temperatures.

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Topics to be Addressed

- - Fundamentals of CSTR with Heat Effects
- - Unsteady-State and Steady-State Energy Balances
- Multiple Steady States (MSS): Analysis and Stability
- - Ignition and Extinction Temperatures
- - Practical Examples and Case Studies

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Objectives



- By the end of this lecture, students will be able to:
- - Understand heat effects in CSTR operation.
- - Analyze unsteady-state and steady-state energy balances.
- Identify and evaluate multiple steady states in CSTRs.
- Apply ignition and extinction concepts to reactor design.

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Introduction



- Understanding the relationship between heat generation and removal is crucial for predicting reactor stability.
- This session delves into steady-state and unsteadystate energy balances, multiple steady states, and the associated temperature profiles.

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CSTR with Heat Effects





Courtesy of Pfaudler, Inc.

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$$\begin{split} \dot{Q} - \dot{W}_{S} + \sum_{i=1}^{n} F_{i0}H_{i0} - \sum_{i=1}^{n} F_{i}H_{i} = \frac{d\hat{E}_{sys}}{dt} \\ \text{Neglect} \\ \text{Using } \hat{E}_{sys} = \sum N_{i}E_{i} = \sum N_{i}(H_{i} - PV_{i}) = \sum N_{i}H_{i} - PV_{i} \\ \frac{dE_{sys}}{dt} = \frac{d\sum N_{i}H_{i}}{dt} = \sum N_{i}\frac{dH_{i}}{dt} = \sum H_{i}\frac{dN_{i}}{dt} \\ \frac{dH_{i}}{dt} = C_{Pi}\frac{dT}{dt} \\ \frac{dN_{i}}{dt} = -\upsilon_{i}r_{A}V + F_{i0} - F_{i} \\ \text{Tikrit University - Equation 2} \\ \end{split}$$



We obtain after some manipulation:

$$\frac{dT}{dt} = \frac{\dot{Q} - \dot{W}_{S} - \sum F_{i0}C_{Pi}(T - T_{i0}) + [-\Delta H_{Rx}(T)](-r_{A}V)}{\sum N_{i}C_{Pi}}$$

Collecting terms with $\dot{Q} = UA(T_a - T)$ and $\dot{W}_s = 0$ high coolant flow rates, and $F_{i0} = F_{A0}\Theta_i$

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$$\frac{dT}{dt} = \frac{F_{A0}}{\sum N_i C_{P_i}} \left[G(T) - R(T) \right]$$

$$G(T) = (r_A V) \left[\Delta H_{Rx} \right]$$

$$R(T) = C_{P_0} \left[(1 + \kappa) T - (T_0 + \kappa T_a) \right]$$

$$R(T) = C_{P_0} \left(1 + \kappa \right) \left(T - \frac{T_0 + \kappa T_a}{1 + \kappa} \right) = C_{P_0} \left(1 + \kappa \right) (T - T_C)$$

$$\kappa = \frac{UA}{F_{A0} C_{P0}} \qquad T_C = \frac{T_0 + \kappa T_a}{1 + \kappa}$$
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$$\frac{dT}{dt} = G(T) - R(T)$$

If G(T) > R(T) Temperature Increases If R(T) > G(T) Temperature Decreases

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Steady State Energy Balance for CSTRs-



At Steady State

$$\frac{\mathrm{dT}}{\mathrm{dt}} = \frac{\mathrm{dN}_{\mathrm{A}}}{\mathrm{dt}} = 0$$

$$-r_{A}V = F_{A0}X$$
$$G(T) - R(T) = \theta$$
$$(-\Delta H_{Rx})F_{A0}X - F_{A0}\sum \Theta_{i}C_{P_{i}}(T - T_{0}) - UA(T - T_{a}) = 0$$

Solving for X.

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Steady State Energy Balance for CSTRs-



Solving for X:

$$X = \frac{\sum \Theta_i C_{P_i} (T - T_0) + \frac{UA}{F_{A0}} (T - T_a)}{-\Delta H_{Rx}^\circ} = X_{EB}$$

Solving for T:

$$T = \frac{F_{A0}X(-\Delta H_{Rx}) + UAT_{a} + F_{A0}\sum \Theta_{i}C_{P_{i}}T_{0}}{UA + F_{A0}\sum \Theta_{i}C_{P_{i}}}$$

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Steady State Energy Balance for CSTRS



$$X(-\Delta H_{Rx}) = C_{P_0} \left[T - T_0 + \frac{UA}{F_{A0}C_{P_0}} (T - T_a) \right]$$

Let
$$\kappa = \frac{UA}{F_{A0}C_{P_0}}$$

$$X(-\Delta H_{Rx}) = C_{P_0} (T + \kappa T - T_0 - \kappa T_a) = C_{P_0} (1 + \kappa) \left(T - \frac{T_0 + \kappa T_a}{1 + \kappa}\right)$$
$$= C_{P_0} (1 + \kappa) (T - T_C)$$

 $\frac{T_{0} + \kappa T_{a}}{\Gamma_{0} + \kappa} = \frac{T_{0} + \kappa T_{a}}{\Gamma_{0} + \kappa}$ 4 Tikrit University جامعة تكريت - Tikrit University

Steady State Energy Balance for CSTRs



$$\underbrace{\frac{G(T)}{-X \Delta H^{o}_{Rx}}}_{=} \underbrace{\frac{R(T)}{C_{P0}(1+\kappa)(T-T_{C})}}$$

$$X = \frac{C_{P0} (1 + \kappa) (T - T_{C})}{-\Delta H^{o}_{Rx}}$$

$$T = T_{C} + \frac{\left(-\Delta H^{o}_{Rx}\right)(X)}{C_{P0}(1+\kappa)}$$

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Steady State Energy Balance for CSTRs





Variation of heat removal line with κ (κ =UA/C_{P0}F_{A0})

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YOUR WAY TO SUCCESS

 $V = \frac{F_{A0}X}{-r_A(X,T)}$

 $A \rightarrow B$

1) Mole Balances:
$$V = \frac{F_{A0}X}{-r_A}$$

2) Rate Laws:
$$-r_A = kC_A$$

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3) Stoichiometry: $C_A = C_{A0} (1 - X)$

4) Combine:

$$V = \frac{F_{A0}X}{kC_{A0}(1-X)} = \frac{C_{A0}v_{0}X}{kC_{A0}(1-X)}$$

$$\tau \mathbf{k} = \frac{\mathbf{X}}{1 - \mathbf{X}}$$

$$X = \frac{\tau k}{1 + \tau k} = \frac{\tau A e^{-E/RT}}{1 + A e^{-E/RT}}$$

$$G(T) = X(-\Delta H_{Rx}) = \frac{\tau A e^{-E/RT}}{1 + A e^{-E/RT}} (-\Delta H_{Rx})$$
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Variation of heat generation curve with space-time.

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Finding Multiple Steady States with T_o varied

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Temperature ignition-extinction curve

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Stability of multiple state temperatures

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MSS - Generating G(T) and R(T)



$$\frac{dT}{dt} = 1$$

$$G(T) = X \cdot (-\Delta H_{Rx})$$

$$R = C_{P_0} \cdot (1 + \kappa) \cdot (T - T_C)$$

Need to solve for X after combining mole balance, rate law, and stoichiometry.

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MSS - Generating G(T) and R(T)

For a first order irreversible reaction

$$\mathbf{X} = \frac{\mathbf{tau} \cdot \mathbf{k}}{\left(1 + \mathbf{tau} \cdot \mathbf{k}\right)}$$

$$\mathbf{k} = \mathbf{k}_1 \exp\left[\frac{\mathbf{E}}{\mathbf{R}}\left(\frac{1}{\mathbf{T}_1} - \frac{1}{\mathbf{T}}\right)\right]$$

Parameters

Tau,
$$(-\Delta H_{Rx})$$
, k_1 , E, R, T_1 , T_C , kappa, C_{P_0}

Then plot G and R as a function of T.

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Are you ready?





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Summary



- In this lecture, we covered:
- Heat effects and energy balance fundamentals for CSTRs.
- - Analysis of multiple steady states and their stability.
- - Concepts of ignition and extinction temperatures.
- - Practical examples to reinforce theoretical concepts.
- Understanding these principles is critical for designing stable and efficient reactor systems.

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